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## THE STUDY OF THE POSSIBILITY OF OBTAINING CHROMITE CONTAINING CONCENTRATE FROM TAILINGS

**Abstract**: The article presents the possibility of additional extraction of chromite concentrate from enrichment tails of chromite containing ores by the gravitational method. The enrichment of chromite-containing sludges by gravity methods - on a concentration table and a KNELSON centrifugal separator have been conducted. Concentration on the table for the class size sludge -0.2 + 0.071 mm obtained chromite concentrate with  $Cr_2O_3$  48.8%, a centrifugal separator KNELSON slurry on the class size -0.0710 mm obtained in open loop chromite concentrate with  $Cr_2O_3$  42.8%;

*Key words*: enrichment, sludge tailings, chromite, concentrate, concentration table, centrifugal separator.

Analysis of the current scientific and technical data shows the increased difficulty in innovative solutions development for metal extraction from different kinds of mineral raw materials, due to fundamental change in mineral resources base of metallurgy. Apart from polymetallic ores, complex in chemistry and intractable, the basis for the current mineral resources base is formed by technogenic production waste. In most cases, technogenic waste is not used, and their use is a threat to the environment. The most dangerous are technogenic wastes containing toxic elements, including sludge tailings of enrichment of chromite-containing ores [1, 2, 3, 4, 12, 13].

A fundamental disadvantage of existing technologies for processing chromite-containing ores is the formation of production waste - sludge stored in ponds - sludge collectors. Modern gravitational technologies of enrichment of chromite-containing ores make it possible to effectively obtain chromite concentrates from large and medium fractions, and fine sludge is practically not enriched due to the difficulty of separating complex minerals into chromite concentrates and waste rock.

The traditional method of enrichment of chromite ores by gravity methods consists in the stage-by-stage crushing and grinding of ore containing chromites to a particle size of 0.5 mm and the use of enrichment operations in heavy liquids, on depositors and (or) on concentration tables [5-8]. However, only large-scale chromite ore with a mass fraction of chromium oxide of 30.0% is subjected to enrichment. Get a concentrate containing 55.0% of chromium dioxide and final tailings with a chromium dioxide content of more than 5.0%. The disadvantage of this method is the low extraction of chromium dioxide in the concentrate, due to the large losses it with tailings - sludge in the form of fine particles and intergrowths. Gravity concentrates can be finished by flotation [9] and magnetic separation [10-11].

Additional extraction of chromium from these technogenic formations, taking into account the existing demand for chromium concentrates, is an important practical task.





For research was used sludge - fine fraction (class -0.2 + 0 mm), tailings of the processing plant of chromite-containing ores of the Republic of Kazakhstan table. 1.2.

Element	Content,%	Element	Content,%
Cr <sub>2</sub> O <sub>3</sub>	25.47	Cu	0.008
Fe <sub>2</sub> O <sub>3</sub>	9.1	Pb	0.05
SiO <sub>2</sub>	21.53	As	0.025
AI <sub>2</sub> O <sub>3</sub>	1.51	Sb	0.23
Н2О(связанная)	7.8	Κ	0.05
CaO	0.75	Na	0.05
MgO	29.4	Р	0.008
MnO <sub>2</sub>	0.053	C	< 0.2
Sобщ	0.1	Ад г/т	< 2.0
S <sub>сульф.</sub>	< 0.1	Аи г/т	< 0.05
Zn	0.1	Ni	0.28
Со	0.02		

Table 1 - Chemical analysis of tailings of the processing plant

Table 2 - X-ray phase analysi	is of sludge tailings
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Phase name	Formula	The content of the phase,%
Antigorite	Mg <sub>3</sub> Si <sub>2</sub> O <sub>5</sub> (OH) <sub>4</sub>	41.8
Clinochrysotile	$Mg_3Si_2O_5(OH)_4$	5.1
Lizardite-1M	$(Mg, Fe)_3Si_2O_5(OH)_4$	12.5
Aluminum Ferrous magnesite	$MgAl_6Fe_{1.4}O_4$	8.7
Chromite	$(Fe_{0.52}Mg_{0.48})Cr_{0.76}(Al_{0.24})O_4$	15.3
Klinohlor	$Mg_6Si_4O_{10}(OH)_8$	5.6
Aluminum Magnesium Silicate	$Ca_{23.20}Mg_{22.4}(Al_{92}Si_{100}O_{384})$	11.0
Quartz	SiO <sub>2</sub>	-

The enrichment of medium and poor in quality of chromite-containing ores and technogenic raw materials is carried out according to the technological scheme of multi-stage extraction of a valuable component as it is discovered, which is based on gravity processes.

In this study, studies were conducted on the gravitational enrichment of sludge of a particle size of -0.2 + 0.071mm on a concentration table and -0.071 + 0 mm on a KNELSON centrifugal concentrator model KS-MD3 of FLSmidth Company.

Data on the enrichment of sludge particle size -0.2 + 0.071 mm on the concentration table are given in Table 4, and on enrichment of the class of paricle size -0.071 + 0 mm on a centrifugal separator are given in Table 5.

With the enrichment of sludge on the concentration table in the open cycle, a chromite concentrate was obtained with a  $Cr_2O_3$  content of 48.8%, with its output of 29.42% and  $Cr_2O_3$  extraction of 73.02% of the operation. The loss of chromium oxide with concentration section tails constitute 18.62%, when the content of  $Cr_2O_3$  6.5%.

In a centrifugal separator KNELSON in open loop obtained chromite concentrate centrifugal separator with a content of  $Cr_2O_3$  42.8%, with 48.5% of its output and extracting  $Cr_2O_3$  66.64% of





the operation. The loss of chromium oxide with centrifugal separator tails is 19.16%, with a  $Cr_2O_3$  content of 15.75%.

Name	Output, %		Content of	Extraction of	Extraction of
	from class	from sludge	Cr <sub>2</sub> O <sub>3</sub> ,%	Cr <sub>2</sub> O <sub>3</sub> ,%	Cr <sub>2</sub> O <sub>3</sub> ,% from
				from class	sludge
Concentrate concentration table	29.42	4.84	48.8	73.02	7.45
Middling concentration table	14.3	2.35	11.5	8.36	0.85
Tails of the concentration table	56.28	9.27	6.5	18.62	1.9
TOTAL	100.0	16.46	15.64	100.0	10.2

Table 4 - Processing of sludge on the concentration table

Table 5 - Sludge	dressing on a	KNELSON	centrifugal	separator
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Name	Output, %		Content of	Extraction of Cr <sub>2</sub> O <sub>3</sub> ,%	
	from class	from sludge	Cr <sub>2</sub> O <sub>3</sub> ,%	from class	from sludge
Main separation concentrate	48.5	32.1	42.8	66.64	55.0
Control separation concentrate	13.6	9.02	32.8	14.2	11.72
Separation tails	37.9	25.08	15.75	19.16	15.80
TOTAL	100.0	66.2	31.14	100.0	82.52

Yield of total concentrate containing 43,58%  $Cr_2O_3$  was 37.0% of the original sludge. Extraction of Cr2O3 in concentrate was 62.45%. The total loss of chromium in the tails and in the class of particle size +0.2 mm will be 24.98%, with its content ~ 12.0%.

The results of gravitational enrichment of sludge show the feasibility of applying the concentration table process for a particle size of -0.2 + 0.071 mm and centrifugal separation for thin size classes (-0.071 + 0 mm).

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